



1 A New Instrument for Time Resolved Measurement of HO₂ Radicals

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5 *Abstract*

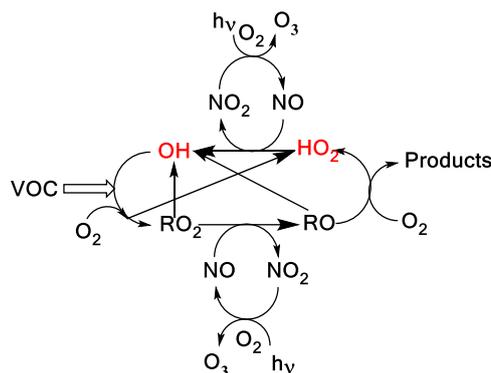
6 OH and HO₂ radicals are closely coupled in the atmospheric oxidation and combustion of volatile
7 organic compounds (VOCs). Simultaneous measurement of HO₂ yields and OH kinetics can
8 provide the ability to assign site specific rate coefficients that are important for understanding the
9 oxidation mechanisms of VOCs. By coupling a FAGE LIF detection system for OH and HO₂ with
10 a high pressure laser flash photolysis system, it is possible to accurately measure OH pseudo-first-
11 order loss processes up to $\sim 100000\text{ s}^{-1}$ and to determine HO₂ yields via time resolved
12 measurements. This time resolution allows discrimination between primary HO₂ from the target
13 reaction and secondary production from side reactions. The apparatus was characterized by
14 measuring yields from the reactions of OH with H₂O₂ (1:1 link between OH and HO₂), with
15 C₂H₄/O₂ (where secondary chemistry can generate HO₂), with C₂H₆/O₂ (where there should be
16 zero HO₂ yield) and with CH₃OH/O₂ (where there is a well-defined HO₂ yield).

17 As an application of the new instrument, the reaction of OH with n-butanol has been studied at
18 293 and 616 K. The bimolecular rate coefficient at 293 K, $(9.24 \pm 0.21) \times 10^{-12}\text{ cm}^3\text{ molecule}^{-1}\text{ s}^{-1}$,
19 is in good agreement with recent literature, verifying that this instrument can both measure HO₂
20 yields and accurate OH kinetics. At 616 K the regeneration of OH in the absence of O₂, from the
21 decomposition of the β -hydroxy radical, was observed, which allowed the determination of the
22 fraction of OH reacting at the β site (0.23 ± 0.04). Direct observation of the HO₂ product in the
23 presence of oxygen has allowed the assignment of the α -branching fractions (0.57 ± 0.06) at 293 K
24 and (0.54 ± 0.04) at 616 K; branching ratios are key to modelling the ignition delay times of this
25 potential ‘drop-in’ biofuel.

26

27 **1 Introduction**

28 In the atmosphere, HO₂ and OH radicals (OH + HO₂ = HO_x) are closely coupled via several
29 reactions as shown in Scheme 1. The short lifetimes of HO_x radicals mean that concentrations are
30 determined by chemical production and removal and not by transport processes, making them ideal
31 candidates as test species for our understanding of atmospheric chemical mechanisms (Stone et
32 al., 2012; Monks, 2005; Stockwell et al., 2012).



33

34 **Scheme 1.** A simplified tropospheric HO_x cycle showing the importance of these short-lived
 35 radical species both to the chemical removal of VOCs and the formation of ozone.

36

37 In Scheme 1, the reaction of alkoxy radicals with molecular oxygen is a major route to HO₂
 38 formation; however, this is not the only significant HO₂ formation process; for example, in the
 39 atmospheric oxidation of n-butanol, HO₂ can be formed via two different mechanisms. Abstraction
 40 by OH at the α position leads to a radical which reacts with oxygen to directly produce HO₂ (R1a,
 41 R2) whereas abstraction at other sites leads to alkylperoxy radical (C₄H₉O₂) formation with varying
 42 fractions of the RO₂ forming alkoxy radicals, and subsequently HO₂ (McGillen et al., 2013) on a
 43 longer timescale.



46 The fraction of alkoxy radicals formed depends on the mechanism of RO₂ removal (reaction with
 47 NO or self or cross-reactions) and the yield of HO₂ from the alkoxy radical depends on the
 48 competition between decomposition, isomerization and reaction with O₂, which in turn will depend
 49 on the structure of the alkoxy radical, temperature, pressure and concentration of oxygen (Orlando
 50 et al., 2003). Therefore, in order to determine the HO₂ yield from the OH initiated oxidation of
 51 compounds such as n-butanol, it is important to have a selective, sensitive and time resolved
 52 method of HO₂ detection.

53 The importance of HO₂ chemistry is not limited to atmospheric processes; HO₂ is a key
 54 intermediate in low temperature (500 – 1000 K) combustion processes, particularly those involving



55 oxygenated fuels (Zador et al., 2011). The mechanisms of low temperature combustion are of
56 particular interest in the development of new engine technologies such as reactively controlled
57 compression ignition (RCCI) (Reitz and Duraisamy, 2015) and are closely linked to atmospheric
58 oxidation mechanisms. Monitoring HO₂ concentrations under the elevated temperatures and high
59 pressures of combustion processes is therefore also of interest. In low-temperature combustion,
60 HO₂ formation is a chain inhibition process, with OH reformation a chain propagating or chain
61 branching process. The ratio of chain branching to chain inhibition processes is often the
62 controlling factor in modelling ignition delay times (Agbro et al., 2017). High temperatures and
63 concentrations of oxygen may be required to convert atmospheric processes, which take several
64 10s of seconds at ambient temperatures (and hence may be influenced by surface chemistry or
65 secondary reactions) to the milli- or microsecond timescale where they can be studied by flash
66 photolysis techniques without such interferences (Medeiros et al., 2018).

67 Direct measurements of HO₂ rely on absorption techniques, and kinetic information on
68 HO₂ reactions has been determined mainly using absorption spectroscopy. This can be achieved
69 either with conventional absorption techniques, often in the UV, (including multipass optics to
70 enhance the pathlength) or in the IR with cavity ring down spectroscopy (CRDS) (Assaf et al.,
71 2018; Onel et al., 2017). However, the HO₂ UV absorption spectrum (200 - 260 nm) is broad and
72 featureless (Crowley et al., 1991), and as such, overlaps with the UV absorptions of many other
73 species present in atmospheric degradation pathways or combustion systems (particularly H₂O₂
74 and RO₂). To utilize the selectivity of the structured IR spectra, absorption methods have been
75 developed in both the mid and near-IR (NIR) (Taatjes and Oh, 1997). Mid-IR absorption features
76 for HO₂ provide sufficient absorption cross-sections for study (Jemialade and Thrush, 1990) but
77 suffer from severe pressure broadening, reducing sensitivity under the conditions relevant to
78 atmospheric and combustion systems (Thiebaud and Fittschen, 2006). Detection in the NIR has
79 similar advantages in terms of a structured spectrum providing greater selectivity; the weaker
80 absorption cross-sections are compensated by the higher powers and ease of use of NIR laser
81 sources (Gianella et al., 2016). However, pressure broadening and interference from H₂O
82 absorptions can make these measurements difficult at even low concentrations of water (10¹⁴
83 molecule cm⁻³).



84 In the atmosphere (Stone et al., 2012) and in chamber studies (Glowacki et al., 2007), HO₂
85 is detected using a sensitive, but indirect method via conversion to OH, with detection of OH via
86 laser induced fluorescence (LIF) (Hard et al., 1984; Brune et al., 1995; Fuchs et al., 2011) or
87 conversion to H₂³⁴SO₄ with subsequent detection of the acid via mass spectrometry (Edwards et
88 al., 2003; Hanke et al., 2002). In the LIF method, also known as Fluorescence Assay by Gaseous
89 Expansion (FAGE (Hard et al., 1984)), which is the technique used in this study, OH is sampled
90 into a low pressure region through a pinhole. Low pressures allow for the temporal separation of
91 resonant 308 nm fluorescence from the excitation pulse. Following the first detection axis for OH,
92 a flow of NO is introduced which reacts with HO₂ (R3):



94 The resulting OH is monitored at a second detector. The high sensitivity with which OH can be
95 detected gives HO₂ detection limits in the 10⁸ molecule cm⁻³ range for 5 – 10 s averaging, however,
96 to extract concentrations, both OH detection methods require calibration (Winiberg et al., 2015).
97 For chamber measurements of HO₂, comparisons with direct CRDS measurements have verified
98 the reliability of the calibration process (Onel et al., 2017).

99 HO₂ detection by LIF can be potentially sensitive to interferences from certain RO₂ species
100 which may also be converted to OH on short timescales. Interferences can be minimized by short
101 conversion times between NO injection and OH monitoring, utilizing low pressures, high flow
102 rates of the sample gas, and low NO concentrations to separate OH generation from HO₂ and RO₂,
103 reduced conversion of HO₂ reduces the sensitivity of this technique and as such in practice a
104 compromise between selectivity and sensitivity is used (Fuchs et al., 2011; Hard et al.,
105 1984; Whalley et al., 2013).

106 The current paper describes a significant development on our earlier FAGE based
107 instrument for time-resolved OH detection (Stone et al., 2016). In this improved system, laser flash
108 photolysis in a high pressure (up to 5 bar), temperature controllable (300 – 800 K) reactor (shown
109 in Figure 1) generated radicals which were then sampled through a pinhole forming a jet within
110 the low pressure detection region (shown in more detail in Figure 2). OH radicals were monitored
111 by LIF close to the pinhole. The jet breaks down after ~20 mm and NO was injected after this
112 point to convert some HO₂ into OH which was then detected by a second monitoring system. In
113 general, LIF becomes less sensitive at higher temperatures (due to distribution of population over



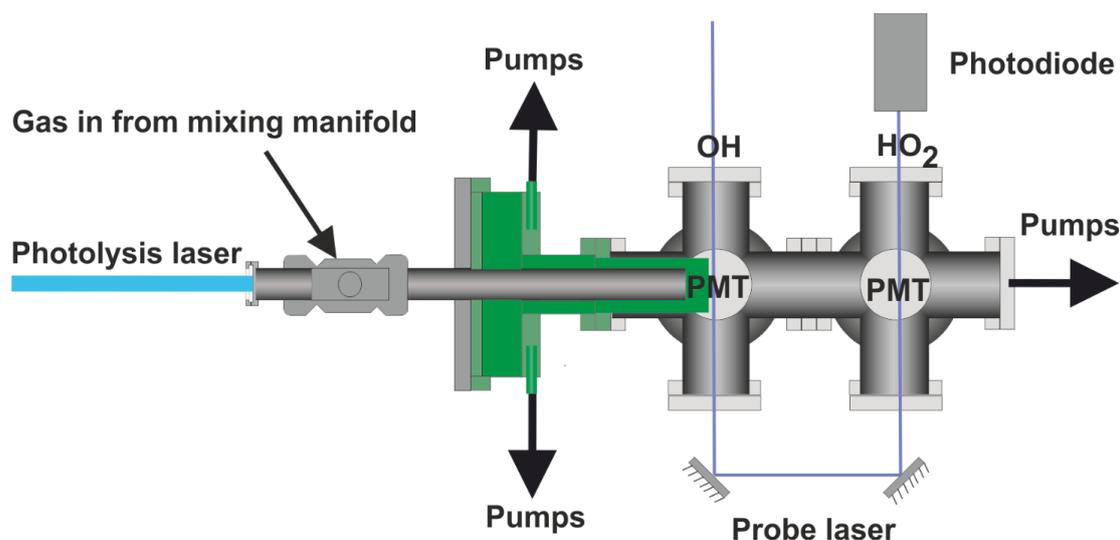
114 more rotational levels) and O₂ concentrations (due to quenching). Sampling into the low-pressure
115 region reduces both the effect of collisional quenching and temperature on the sensitivity of LIF
116 detection, although there is a reduction in the number density of the HO_x species in the expansion.
117 We report the adaptation of our time-resolved OH-FAGE instrument to allow HO₂ detection, the
118 characterization of the instrument (including development of a calibration method for HO₂ yields
119 of OH initiated reactions), and the investigation of the influence of RO₂ species. Finally, we discuss
120 the application of the technique to determine the yield of HO₂ from the reaction of OH with n-
121 butanol.

122

123 **2 Experimental**

124 Reactions were carried out in a high pressure (0.5 – 5 bar) reaction cell which is described in
125 greater detail in Stone et al. (2016) and schematics of which are shown in Figures 1 and 2. The
126 high-pressure reactor was a 0.5 m stainless steel tube with a 22 mm internal diameter. Gas flows
127 were delivered to the high-pressure cell from a mixing manifold where calibrated mass flow
128 controllers (MFC) allowed for accurate control of flow rates. Low vapour pressure compounds:
129 OH precursors (H₂O₂), and substrates methanol and butanol, were delivered to the mixing manifold
130 from, thermostatted bubblers in pressure regulated backing flows of nitrogen (N₂). Ethane and
131 oxygen were delivered directly from cylinders into the mixing manifold through MFCs. The gas
132 flowrate through the cell was kept under laminar conditions with typical Reynolds values (Re) of
133 480 (corresponding to a flow rate for an experiment of 10 SLM at 2 bar); in general conditions
134 were maintained between 400-800 Re (Re < 2400 = laminar flow), with some experiments carried
135 out with higher flowrates, up to 1800 Re.

136 Temperature control of the reactor between room temperature and 800 K was achieved by
137 altering the voltage applied to a coil heater (WATROD tubular heater, Watlow) over the last 30
138 cm of the stainless-steel tube. The heated region was fitted with a quartz liner (inner diameter 18
139 mm) to reduce wall-initiated chemistry. A temperature readout, from a type K thermocouple in the
140 gas flow, close to the pinhole, was calibrated for given flow rates, pressures and voltage settings
141 by measuring the highly temperature sensitive OH and methane rate coefficient, using the
142 temperature dependence reported by (Dunlop and Tully, 1993). A more detailed description of
143 this method is described within instrument characterization (Section 3.4).



144

145 **Figure 1.** Schematic plan of the apparatus.

146

147 The photolysis of the OH precursor, H₂O₂, at 248 nm (Lambda Physik, Compex 200
148 operated using KrF) or 266 nm (frequency quadrupled Nd-YAG output, Quantel, Q-smart 850)
149 initiated the chemistry.



151 Hydrogen peroxide was used as the OH precursor for all experiments where HO₂ detection was
152 performed, because it also acts as an internal calibrant to relate OH and HO₂, via reaction R5:



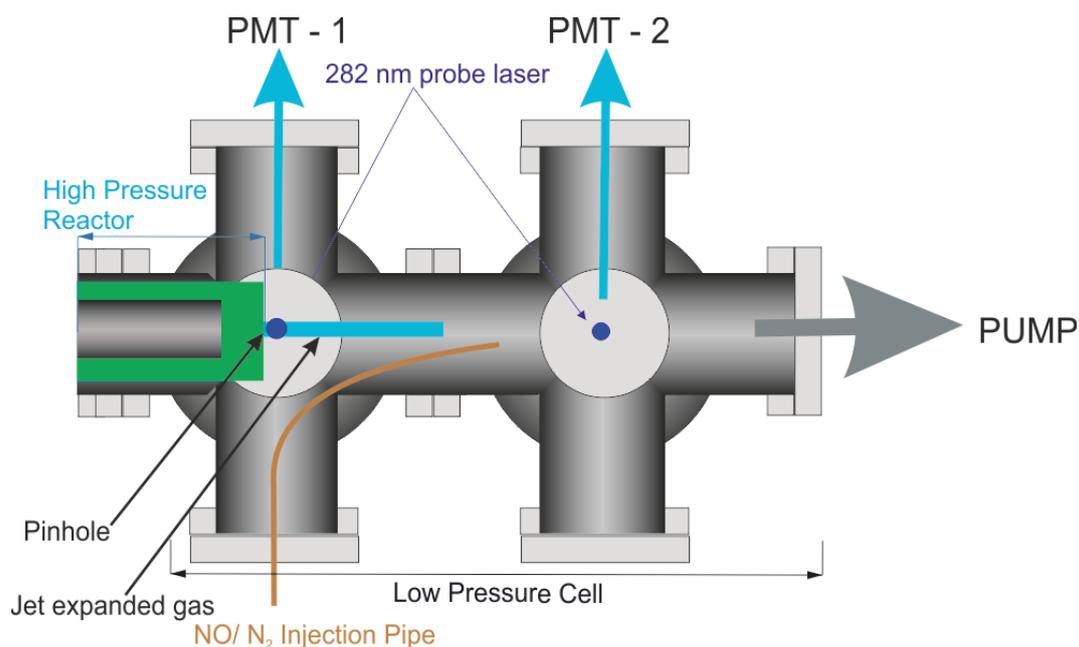
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155 However, in general, other OH precursors can be used. The OH precursor was maintained at low
156 concentrations ($1 \times 10^{14} - 1 \times 10^{15}$ molecule cm⁻³) to minimise errors associated with assigning
157 pseudo-first-order kinetics for the loss of OH, and to reduce radical-radical reactions. Maintaining
158 a low radical precursor concentration had the additional advantage of minimising attenuation of
159 the photolysis beam, ensuring consistency in the initial radical concentrations generated along the
160 length of the high-pressure cell. Initial OH concentrations were in the range $2 \times 10^{11} - 5 \times 10^{13}$
161 molecule cm⁻³.



162 A pinhole (diameter < 0.15 mm) at the end of the high-pressure reactor couples the reactor
163 to the low-pressure (0.3 – 5 Torr) detection cell. Details on OH detection can be found in Stone et
164 al. (2016). The accuracy of the instrument for OH measurement has recently been verified by
165 measurements of the rate coefficient of the reaction of OH with isoprene (Medeiros et al., 2018)
166 which are in excellent agreement with the literature. A more detailed schematic for the low-
167 pressure detection cell is shown in Figure 2.

168



169

170 **Figure 2.** Detailed schematic elevation of the low-pressure detection region of the reactor. The
171 blue line represents the jet expanded gas; the jet breaks down after approximately 2 cm. NO was
172 injected through a 1.5 mm id stainless steel tube after the breakdown of the jet.

173

174 In the first low pressure detection cell, the OH was probed within the jet expanded gas,
175 close to pinhole (< 5 mm), perpendicular to the gas flow. The OH was detected by off-resonance
176 laser induced fluorescence (LIF) at 308 nm following excitation with 282 nm light ($A^2\Sigma(v' = 1)$
177 $\leftarrow X^2\Pi(v'' = 0), Q_{11}$). The 282 nm light was the frequency doubled output of a dye laser
178 ((Rhodamine 6 G, Spectron) pumped at 532 nm by a Nd:YAG laser (Spectron), or (Rhodamine 6
179 G, Continuum) pumped by a Nd-YAG laser (Quantel, Q-smart 850)). Measuring the off-resonance



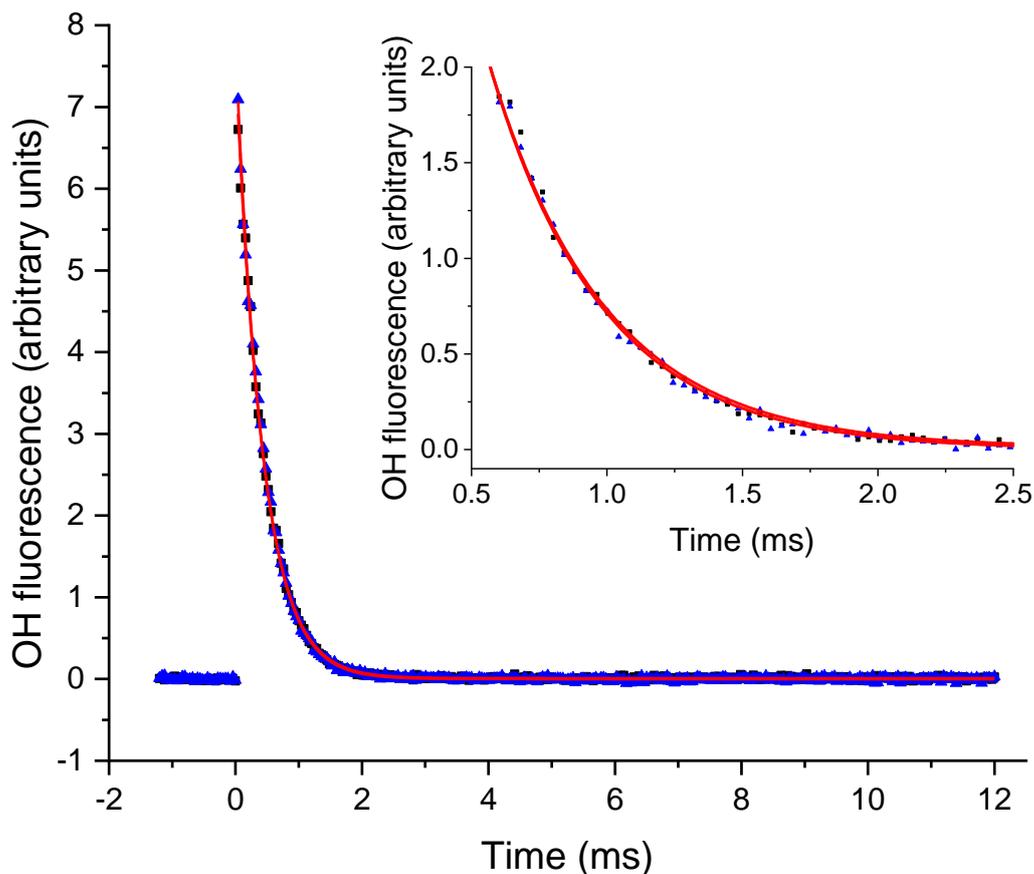
180 fluorescence allowed the use of a filter (308 ± 5 nm, Barr Associates) before the photomultiplier
181 (Perkin-Elmer C1943P) to remove scattered light and improved the signal to noise ratio.

182 A delay generator (BNC DG535) was used to vary the delay between the photolysis and
183 probe laser, facilitating generation of time profiles of the OH concentration. The traces were
184 scanned through multiple times (5 – 20) and the signal at each time point was averaged, giving
185 high precision OH loss traces. An example OH trace from the first detection cell for reaction R5
186 is presented in Figure 3. As reactions were carried out under pseudo first order conditions ($[\text{OH}]$
187 \ll [substrate]), the time dependence of the OH LIF signal, I_t , (proportional to the $[\text{OH}]$) was given
188 by:

189
$$I_{f,t} = I_{f,0} e^{-k_{\text{OH}} t}$$

190 where $k_{\text{OH}} = k_5[\text{H}_2\text{O}_2]$. In Figure 3 two traces are presented from the first, OH, detection axis, these
191 two traces were taken in consecutive experiments with a constant $[\text{H}_2\text{O}_2]$ where the first trace
192 ($k_{\text{OH},1\text{st}} = (2351 \pm 22) \text{ s}^{-1}$) was taken where N_2 was flowed into the low pressure region, the second
193 trace ($k_{\text{OH},1\text{st}} = (2389 \pm 18) \text{ s}^{-1}$) was taken when this flow had been switched to NO to allow HO₂
194 detection in the second detection cell, errors are given as 2σ . The similarity of the OH decay traces
195 when either N_2 or NO was injected shows that there was no back streaming of NO in the low-
196 pressure cell and hence no HO₂ conversion at the first detection axis.

197 HO₂ radicals were monitored by the chemical transformation of HO₂ to OH via reaction
198 with NO (R3) in the low-pressure cell. Following the breakdown of the jet, after the Mach disk
199 (>2 cm beyond the pinhole), a small flow (5 sccm) of NO or N_2 was introduced into the low-
200 pressure cell via a 1.5 mm i.d. stainless steel pipe (for a typical 0.5 Torr pressure in the FAGE cell
201 the NO concentration was $5.5 \times 10^{13} \text{ molecule cm}^{-3}$). After passing through the first detection cell,
202 the probe beam was redirected through the second low-pressure detection cell downstream of the
203 NO pipe allowing for the measurement of the OH concentration by LIF in the same manner as in
204 the first cell.



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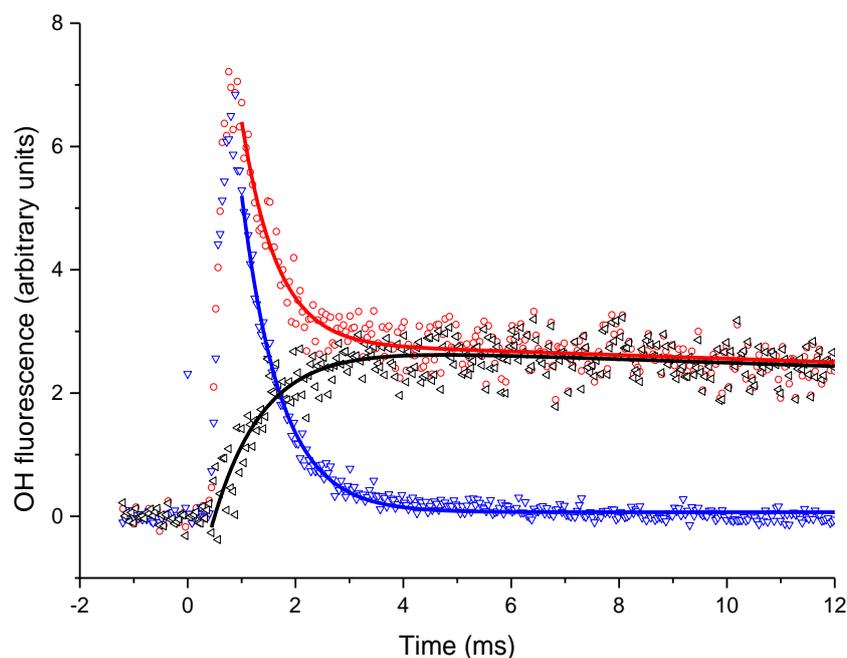
206 **Figure 3.** An example of the OH signal (blue triangles) collected at the first detection axis for the
207 reaction of OH with H₂O₂ ([H₂O₂] ≈ 1.4 × 10¹⁵ molecule cm⁻³, with a flow of N₂ into the low-
208 pressure cell, with black squares representing the subsequent trace taken with a flow of NO. The
209 red lines represent the non-linear least squares fits to an exponential decay ($k_{\text{OH},1\text{st}} = (2351 \pm 22) \text{ s}^{-1}$
210 and $k_{\text{OH},1\text{st}} = (2389 \pm 18) \text{ s}^{-1}$), 2 σ errors.

211

212 By switching between a flow of N₂ and NO, through the pipe, traces for OH loss and HO₂
213 formation could be elucidated, examples of which are shown in Figure 4. Subtraction of the two
214 OH traces in Figure 4, (upper, red trace is with NO injection and the signal corresponds to reactant
215 OH and OH produced from the titration of HO₂ to OH, lower, blue trace with N₂ injection is
216 reactant OH only) gave a resultant signal associated with HO₂ production in the high-pressure
217 reactor, shown the pink trace in Figure 4. The signal from the first PMT allowed for correction of



218 the signal heights at the second PMT for changes in the probe laser power or wavelength, any
219 variations in laser power or wavelength affect the absolute signal retrieved from both PMTs;
220 however, the relative signals retrieved from the PMTs remain consistent.



221

222 **Figure 4.** Examples of OH fluorescence traces collected at the second detection axis under the
223 same conditions for Figure 3. The blue triangles are where N₂ has been injected through the pipe,
224 i.e. no HO₂ to OH conversion. The OH signal profile differs from that in Figure 3, with $k_{\text{OH},2\text{nd}} =$
225 $(1390 \pm 44) \text{ s}^{-1}$ (2 σ errors), additionally, there is a time-delay to peak OH, representing the
226 transport time (primarily the time taken to travel from the breakdown of the jet to the second
227 detection axis). The red circles are the OH signal obtained with NO injection. At short times the
228 signal is dominated by reactant OH, but at times greater than 2 ms, the signal is dominated by OH
229 titrated from the HO₂ product. The resultant OH trace associated with HO₂ formation in the high-
230 pressure cell obtained by subtracting the two OH traces, obtained with either NO or N₂ injection
231 prior to the second detection axis, shown as black triangles, a biexponential growth and decay fit,
232 black curve, gave a formation rate coefficient, $k_{\text{HO}_2,2\text{nd}} = (1080 \pm 150) \text{ s}^{-1}$ (2 σ error).

233

234 Fits to the HO₂ formation traces and OH loss traces from the second cell generated kinetic
235 parameters which differed from the accurate parameters collected at the first detection axis, $k_{\text{OH},2\text{nd}}$



236 = $(1390 \pm 44) \text{ s}^{-1}$ and $k_{\text{HO}_2,2\text{nd}} = (1080 \pm 150) \text{ s}^{-1}$ where the accurate loss parameters from the first
237 cell were $k_{\text{OH},1\text{st}} = (2389 \pm 18) \text{ s}^{-1}$, 2σ errors. This difference was the result of transport effects. By
238 comparison of the loss and formation parameters derived for $\text{OH} + \text{H}_2\text{O}_2$, for the first and second
239 detection cells, HO_2 formation rates could be assigned from a calibration plot (Figure 7).

240 Neither of the OH determinations in the two detection axes provide absolute measurements
241 of radical concentrations. Each detection axis could be calibrated as for chamber measurements,
242 but for our purposes a calibration reaction linking photolytically produced OH and HO_2 removes
243 many sources of error compared to an absolute calibration. The reaction of OH with the radical
244 precursor H_2O_2 which directly forms HO_2 with a 100 percent yield was used for calibration.



246 For reactions carried out where a reagent was added in addition to the H_2O_2 , the resulting ratios
247 can be compared with those from the calibration reaction to allow assignment of an observed HO_2
248 yield. To assign the HO_2 yield from the test reaction required accounting for secondary HO_2
249 production in the high-pressure reactor, from $\text{OH} + \text{H}_2\text{O}_2$ and photolysis processes. From the
250 known rate coefficients, it was possible to calculate the fraction of OH reacting with the H_2O_2 and
251 hence the expected contribution to the HO_2 signal. Photolytic production of HO_2 was accounted
252 for by measuring the observed HO_2 signal in the absence of any H_2O_2 .

253 In a typical experiment, the reaction of OH and H_2O_2 would be carried out four times, twice
254 in the absence of NO and twice with the addition of NO to calibrate the instrument. Exponential
255 fits to the OH decay as monitored in the first cell determine the peak OH signal. The OH signals
256 at the second detector recorded with only N_2 addition (reagent OH reaching the second detector)
257 and subtracted from the signal with NO added (reagent OH and HO_2) to give the net HO_2 signal.
258 This profile was fitted to, a biexponential growth and decay function, to extract the peak HO_2
259 signal for that set of conditions. Combinations of traces were then used to obtain an averaged value
260 (and uncertainty) of the signal on the first PMT (OH) to the net HO_2 signal at the second PMT for
261 this calibration reaction where OH reactant and HO_2 product have a 1:1 relationship. The same
262 process was then performed in the presence of the compound of study. The removal pseudo-first-
263 order rate coefficient with H_2O_2 and the reagent of study ($k'_{\text{OH},1\text{st}} = k_{\text{OH}+\text{H}_2\text{O}_2}[\text{H}_2\text{O}_2] +$
264 $k_{\text{OH}+\text{TEST}}[\text{TEST}]$) was compared to the removal pseudo-first-order rate coefficient with only H_2O_2



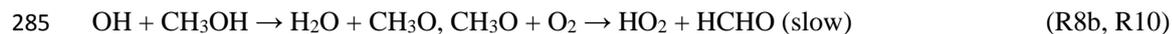
265 ($k_{\text{OH,1st}}^{\text{OH}} = k_{\text{OH}+\text{H}_2\text{O}_2}[\text{H}_2\text{O}_2]$) to assign what fraction of the OH reacted with the H_2O_2 precursor and
266 hence the resulting contribution to the observed HO_2 . Comparison of the remaining peak ratio to
267 the ratio from the H_2O_2 and OH calibration experiment provided the experimentally derived HO_2
268 yield for reaction of OH and the reagent of study.

269 Branching ratios to direct HO_2 formation could be assigned with an accuracy of $\sim 10\%$, the
270 limitations to this were signal to noise effects, where improved signal to noise could be achieved
271 by increasing the precursor concentration and photolysis energy. However, this was limited by the
272 need to ensure pseudo-first-order conditions were maintained and to minimize radical-radical
273 processes. Ensuring the dominant reaction was between OH and the reagent of study, whilst still
274 being able to accurately measure the initial OH conditions, provided a limit to the maximum
275 removal rates achievable ($k_{\text{OH,1st}} < 30,000 \text{ s}^{-1}$).

276

277 3 Instrument Characterization

278 Many reactions of atmospheric and combustion interest are studied in the presence of oxygen
279 leading to the generation of peroxy radicals (RO_2). For certain RO_2 there is a potential to generate
280 OH and HO_2 on a fast timescale and therefore three well known reactions were chosen to
281 characterize the instrument, OH and ethane, OH and ethylene, and OH and methanol.



286 OH and ethane (R6) gives an assessment of any false yields generated from RO_2 and NO from
287 prototypical alkyl RO_2 species that will be formed from many atmospherically relevant reactions.
288 Ethylene and OH (R7) forms a hydroxy alkyl peroxy radical, the typical RO_2 species known to
289 create interferences in FAGE HO_2 detection systems (Fuchs et al., 2011; Hard et al., 1984; Whalley
290 et al., 2013). Minimizing and understanding the HO_2 yield from this reaction allowed for limits to
291 the selectivity of the instrument to be known. The reaction of OH with methanol is a well



292 understood reaction; the two isomeric radical products react with oxygen on differing timescales
293 to generate HO₂. Complete conversion of both isomers should yield 100 % HO₂.

294 As discussed in the experimental section, transport effects after the breakup of the sampling
295 jet mean that rate coefficients measured in the second cell $k_{X,2nd}$ ($X = OH$ or HO₂) differ from each
296 other (transport effects scale with mass) and from those made in the first detection axis ($k_{OH,1st}$).
297 Pseudo-first-order rate coefficients from the two detection axes were compared to ascertain
298 whether measurements in the second detection axes can be used to make quantitative kinetic
299 measurements.

300 Finally, the layout of the apparatus makes it hard to accurately measure the temperature at
301 which the reaction occurs; for reactions occurring on a millisecond timescale, the relevant reaction
302 distance from the sampling pinhole is approximately 0.05 - 0.5 mm. Compared to a conventional
303 slow flow laser flash photolysis/laser induced fluorescence apparatus, where the reaction volume
304 is the overlap of the perpendicular photolysis and probe laser beams, it is hard to accurately
305 position the thermocouple and additionally, any thermocouple located close to the sampling
306 pinhole may affect the flow into the low pressure system. In addition to the difficulties in correctly
307 siting a thermocouple, there are additional errors (flow, conduction and radiative) that derive from
308 measuring the temperature of a flowing gas with a thermocouple. We have therefore performed
309 additional experiments to determine the temperature based on the well characterized and
310 temperature sensitive reaction of OH and methane.

311

312 **3.1 Interference by RO₂ species**

313 Selectivity in measuring HO₂ concentrations plays an important role in the viability of detection
314 methods for monitoring reactions important for atmospheric chemistry. At high pressures, the
315 reaction of NO with many atmospherically relevant RO₂ species in the presence of oxygen induces
316 HO₂ formation. By performing the titration in the low-pressure cell with the NO + HO₂ reaction
317 under ‘starved NO’ conditions minimized this effect. This premise was validated by measuring the
318 OH + ethane and OH + ethylene HO₂ yields under high oxygen conditions. In our system the
319 typical oxygen concentrations in the high pressure reactor were varied between 1×10^{16} and $5 \times$
320 10^{17} molecule cm⁻³ which led to concentrations in the low pressure cell of 3×10^{12} to 2×10^{15}
321 molecule cm⁻³.



322 The reaction of OH + ethane (R6) under high oxygen conditions permits the rapid
323 formation of the ethylperoxy radical, which is an RO₂ radical that has a typical slow, NO
324 propagated, route to HO₂ formation (R11 – R12).



326 ($k_{11, 298 \text{ K}} = 8.70 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$) (Atkinson et al., 2006)



328 ($k_{12, 298 \text{ K}} = 9.48 \times 10^{-15} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$) (Atkinson et al., 2006)

329 Under a variety of NO flows the apparent HO₂ yield for the OH + C₂H₆ system was $3 \pm 6 \%$, which
330 indicates that for most reactions carried out in our system, chemical transformation by reaction
331 with NO, was sensitive to HO₂ rather than RO₂ species, where the RO₂ radical was the product of
332 O₂ addition to a simple alkyl radical.

333 The reaction of ethylene and OH (R7) in the presence of oxygen forms the
334 hydroxyethylperoxy radical (HOCH₂CH₂O₂), and reaction of the HOCH₂CH₂O₂ with NO in the
335 presence of O₂ provides a route for the prompt regeneration of OH. For this reaction, an apparent
336 HO₂ yield of $100 \pm 15 \%$ was observed; however, by varying the concentration of NO added to
337 low pressure cell (between 5×10^{13} and $5 \times 10^{14} \text{ molecule cm}^{-3}$), the formation rate of OH was
338 reduced minimizing the apparent yield observed ($<70 \%$) and slowing the observed rate of OH
339 regeneration ($<1000 \text{ s}^{-1}$).



341 ($k_{13, 298 \text{ K}} = 9.00 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$) (Atkinson et al., 2006)



343 ($k_{14, 298 \text{ K}} = 1.3 \times 10^5 \text{ s}^{-1}$) (Orlando et al., 1998)



345 ($k_{9, 298 \text{ K}} = 9.60 \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$) (Atkinson et al., 2006)

346 For test reagents which can generate radicals similar to hydroxyethylperoxy, our instrument will
347 detect both HO₂ and RO₂ with some selectivity to HO₂.

348

349

350 **3.2 OH + methanol**

351 To verify the accuracy of the method for determining HO₂ yields the reaction of OH and methanol
352 (R8) was examined. The branching ratio for the α abstraction to yield CH₂OH (R8a) reported by
353 the IUPAC evaluation and based on the experimental data of McCaulley et al. (1989), is
354 $\alpha = (85 \pm 8)\%$ at room temperature with the methoxy yield as $(15 \pm 8)\%$. Reaction R8 was studied
355 at room temperature with the reaction being initiated by the photolysis of H₂O₂ at 248 nm. In the
356 presence of low concentrations of oxygen ($< 1 \times 10^{16}$ molecule cm⁻³), the α abstraction still
357 leads to prompt formation of HO₂ via R9, but R10, CH₃O + O₂, occurs on a much longer timescale
358 and is not observed under these conditions. The observed HO₂ yield, $(87 \pm 10)\%$ (first row of Table
359 1) gives the fraction of reaction R8 forming CH₂OH and the value is consistent with the IUPAC
360 evaluation.

361 **Table 1.** HO₂ yields from the reaction of OH with CH₃OH with varying [O₂] carried out 295 K.
362 Errors given as 2 σ .

[O ₂]/ molecule cm ⁻³	HO ₂ Yield (%)				Average HO ₂ Yield (%)
	Expt 1	Expt 2	Expt 3	Expt 4	
$< 1 \times 10^{16}$	90	89	79	88	(87 ± 10)
$> 2 \times 10^{18}$	93	94	100	99	(97 ± 6)

363

364 When higher concentrations of oxygen are used, the timescale for HO₂ production from
365 reaction R10 decreases and now both abstraction channels lead to HO₂ detection in our apparatus.
366 The resulting observed yield (second row of Table 1) is consistent with 100% conversion of OH
367 to HO₂. The reproduction of the literature HO₂ yields from the reaction of OH with methanol under
368 varying [O₂] demonstrates that the instrument can accurately measure HO₂ yields with good
369 precision. It has additionally been demonstrated that the instrument had sufficient accuracy and
370 precision to assign the branching ratios for differing abstraction channels when it was possible to
371 separate the channels by the timescale for HO₂ generation.

372

373



374

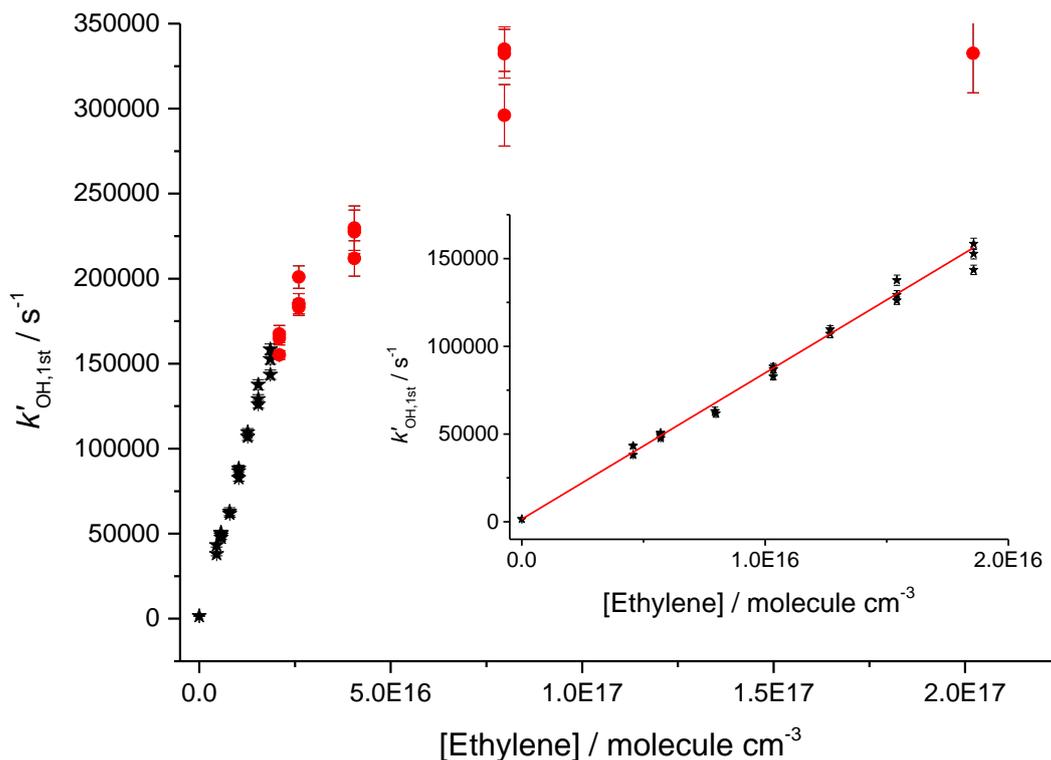
375 **3.3 Assessment of transport effects on observed kinetics**

376 Due to the differing conditions in the two detection regions, the kinetics observed at the first
377 detection axis, where OH LIF was performed in the jet-expanded gas, and in the second detection
378 region, where LIF is performed 15 cm downstream from the pinhole after the breakdown of the
379 jetting gas, will be treated separately. For validating the accuracy of the OH kinetics in the first
380 cell, the reactions of OH and methane (CH₄) (Dunlop and Tully, 1993), OH and ethylene (C₂H₄)
381 (Atkinson et al., 1982; Tully, 1983) were studied. The high accuracy and precision of this system
382 for measuring OH kinetics has further been demonstrated in a recent publication on the reaction
383 of OH and isoprene (C₅H₈) (Medeiros et al., 2018).



387 When these reactions were carried out at room temperature the expected bimolecular rate
388 coefficients could be reproducibly accurately measured for observed rate coefficients less than
389 150,000 s⁻¹.

390 Studies on the reaction of OH and ethylene at room temperature and 2.2 bar, shown in
391 Figure 5, gave a value of $k_7 = (8.33 \pm 0.16) \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$ (2σ errors) which matched
392 well with literature high pressure limits for OH and ethylene; where a direct pulsed laser photolysis
393 laser induced fluorescence study by Tully (1983) gave $k_7 = (8.47 \pm 0.24) \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1}$
394 s⁻¹, and a relative rate study by Atkinson et al. (1982) found $k_7 = (8.11 \pm 0.37) \times 10^{-12} \text{ cm}^3$
395 molecule⁻¹ s⁻¹. However, for pseudo-first order rate coefficients above ~150000 s⁻¹, there was no
396 longer a linear dependence of the rate coefficient with reagent concentration; transport effects are
397 becoming significant even for OH detection in the jetting region.



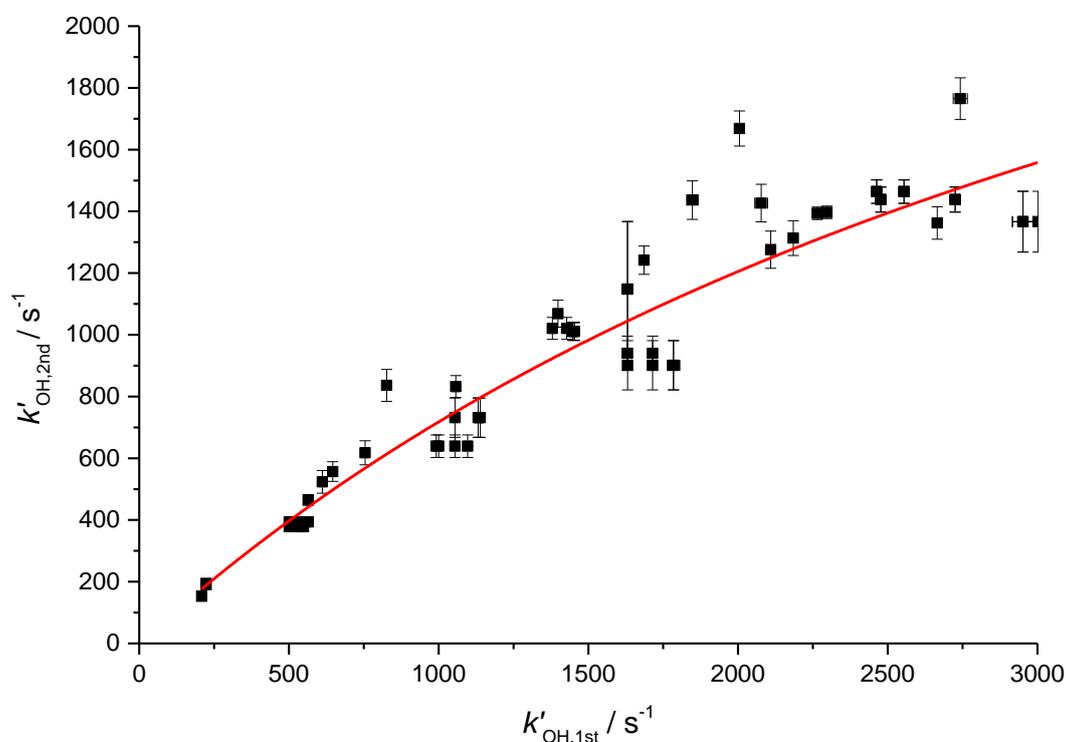
398
399 **Figure 5.** Bimolecular plot of the pseudo-first-order rate coefficient at the first detector, $k'_{\text{OH},1\text{st}}$,
400 vs ethylene concentration. The figure demonstrates a linear relationship below $\sim 150,000 \text{ s}^{-1}$ (see
401 inset for detail in linear region) but with increasing curvature, due to transport effects at higher
402 values of $k'_{\text{OH},1\text{st}}$. Black stars symbolize where $k'_{\text{OH},1\text{st}}$ was linear with $[\text{C}_2\text{H}_4]$, red circles where
403 $k'_{\text{OH},1\text{st}}$ showed greater than 5% deviation from linearity.

404

405 The OH traces detected in the second cell deviated from those observed from the first cell,
406 as shown in Figures 3 and 4. There is understandably an increased time delay from time zero (the
407 photolysis laser pulse) to arrival of OH radicals at the second detection axis due to the increased
408 distance travelled after sampling ($> 150 \text{ mm}$ versus $< 5 \text{ mm}$). Additionally, the arrival of OH to
409 the second axis is spread out further in time due to transport issues relating to non-linear flow
410 conditions at the breakdown of the jet, and the arrival of the OH being affected by its velocity
411 distribution (Moore and Carr, 1977; Taatjes, 2007; Baeza-Romero et al., 2012). Figure 6 shows a
412 plot of observed OH rate coefficient from the first detection axis ($k_{\text{OH},1\text{st}}$) against observed rate
413 coefficient from the second axis ($k_{\text{OH},2\text{nd}}$). For values of k_{OH} below 2500 s^{-1} it was possible to



414 accurately assign an expected OH removal rate for reactions observed in the second cell ($k_{\text{OH},2\text{nd}}$)
415 given the observed OH kinetics at the first detection axis ($k_{\text{OH},1\text{st}}$). This is useful to compare the
416 kinetics of OH removal and HO₂ production.



417

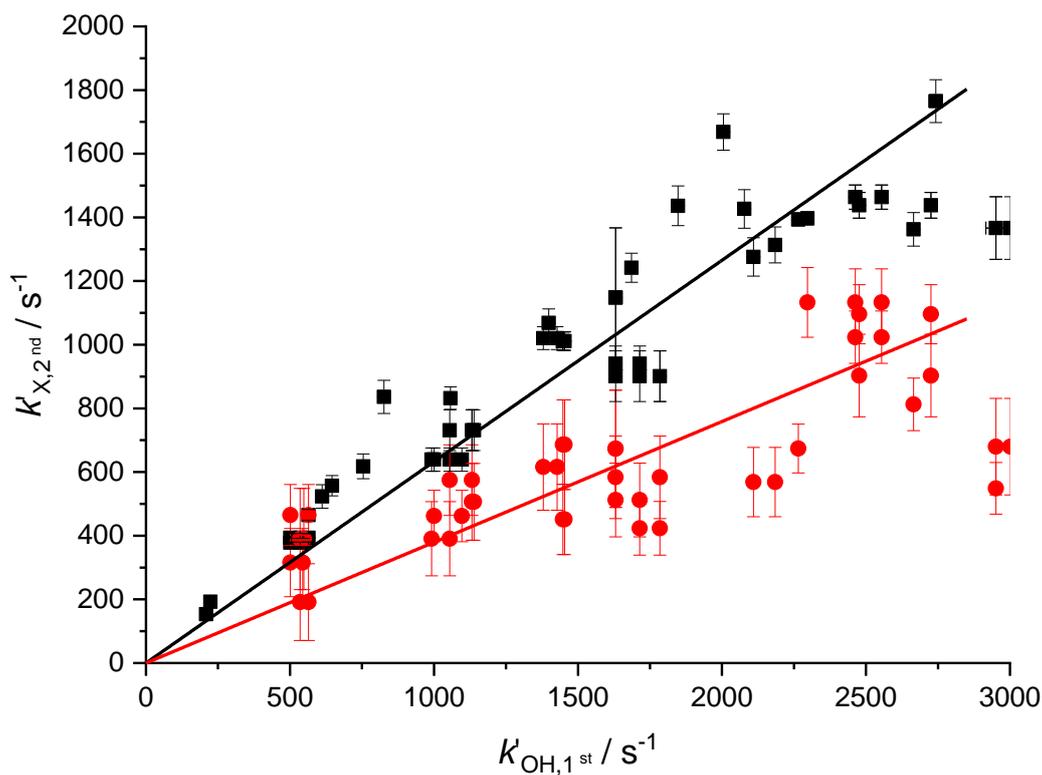
418 **Figure 6.** Relationship between the observed rate coefficient observed in the first cell ($k_{\text{OH},1\text{st}}$) and
419 the observed OH removal rate in the second cell ($k_{\text{OH},2\text{nd}}$). The difference is non-linear but a simple
420 fit to this could be used to assign removal rates to traces observed in the second cell below 2,500
421 s⁻¹. The red line is the simplified fit of the form, $y = A * (1 - e^{-b*x})$, where A was some limit
422 value above which no increase in measured rate coefficient would be observed.

423

424 As the observed kinetics in the second cell are significantly affected by the velocity
425 distribution of the species being detected, there is again a deviation between the observed kinetics
426 expected from the measurement of the OH radicals loss and the kinetics for HO₂ formation due to
427 the differing masses of OH and HO₂. Figure 7 shows the pseudo-first order rate coefficients for
428 OH removal ($k'_{\text{OH},2\text{nd}}$) and HO₂ production ($k'_{\text{HO}_2,2\text{nd}}$) determined at the second detection axis,
429 plotted against the OH removal at the first detection axis. The two fits to the data shown in Figure



430 7 had a ratio of gradients concordant with the root of the masses for HO₂ and OH, 0.60 ± 0.14
431 versus the expected relationship of 0.73. As with Figure 6, it is possible to establish a calibration
432 graph that relates the kinetics of HO₂ production at the second detection axis with the primary
433 kinetics taking place in the high pressure reactor. This means that the timescale over which the
434 HO₂ yield was observed could be assigned and therefore it is possible to attribute HO₂ yields to
435 fast processes, intramolecular RO₂ decompositions or R + O₂ reactions, or to slower radical-radical
436 reactions.



437

438 **Figure 7.** Relationship between the pseudo-first-order rate coefficient for OH loss observed in the
439 first cell ($k'_{\text{OH},1\text{st}}$) and the observed rate coefficients in the second cell ($k'_{\text{X},2\text{nd}}$ where X = OH or
440 HO₂) a non-linear fit can be used to assign removal rates and HO₂ formation rates to traces
441 observed in the second cell below $2,500 \text{ s}^{-1}$.

442

443

444



445 3.4 Temperature corrections

446 It is difficult to know the exact temperature at the pinhole as introducing a thermocouple close to
447 the region will affect the flows and cannot be used in routine operation. A translatable
448 thermocouple was passed along the axis of the high-pressure reactor over a variety of temperatures
449 and showed that the temperature of the gas at the pinhole varies with axial location. In addition,
450 radial profiles showed that in our system there was insufficient heating length to achieve uniform
451 radial heating of the laminar gas. From the axial measurements it was observed that slower flow
452 rates (< 5 SLM) allowed for reduced axial temperature gradients. However, these measurements
453 showed that the only manner to achieve an even thermal profile would be a static cell.

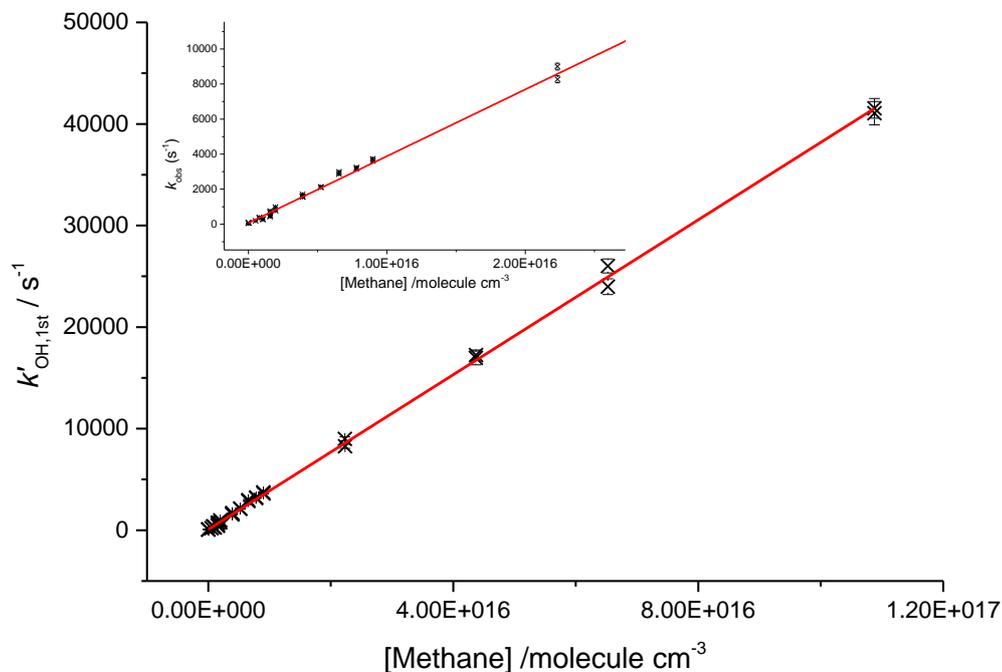
454 A permanently seated thermocouple was placed perpendicularly to the flow, close to the
455 sampling region, measurements from this thermocouple were then compared with temperature
456 assignments from the reaction of OH and methane using the temperature dependence assigned by
457 Dunlop and Tully (1993). This was performed over a range of heater settings and flows to allow
458 for temperature assignment. This method was also applied to a standard low-pressure cell where
459 the flows can be reduced to slow enough flows that thermocouple measurements could accurately
460 define the temperature to verify the method. Additionally, the well-determined OH + ethylene
461 adduct formation equilibrium was measured over a range of temperatures to provide an additional
462 verification of the temperature assignment.

463 The method to assign a temperature from the reaction of OH and methane used the pseudo-
464 first order rate coefficients ($k'_{\text{OH,1st}}$) measured at the first detection axis over a range of added
465 methane flows. An estimate of the temperature was made from the thermocouple measurement,
466 this estimated temperature was used, along with the pressure in the reactor, to calculate the added
467 methane concentration. Comparing the predicted pseudo-first-order rate coefficient that this
468 estimated concentration provided using the literature value of $k_{\text{OH+CH}_4}$ (Dunlop and Tully, 1993) to
469 the measured rate coefficient produced a difference for each point. The estimated temperature was
470 then iteratively changed to minimize the difference between estimated and measured rate
471 coefficients. For this minimum value, the difference between thermocouple measurement and
472 actual temperature was tabulated against the voltage setting for the heater. A parameterization of
473 voltage versus temperature difference was used to estimate the temperature of the reactor for
474 experiments where no OH and methane measurements were performed and has been shown to



475 reliably predict the temperature of the reactor within 7 K when measurements have been made
476 subsequently.

477 To assess the axial temperature gradients in the gas sampled through the pinhole over the
478 timescales of reactions measured, OH and methane rate coefficients were measured using
479 photolysis of water at 193 nm as a source of OH. Using water photolysis allowed for low removal
480 rates of OH by precursor and assignment of OH and methane over a range of pseudo-first-order
481 rate coefficients ($k'_{\text{OH},1\text{st}}$) 100 – 40000 s^{-1} as shown in Figure 8. This was performed at two
482 temperatures (505, 680 K), and the slope of observed OH removal rate coefficients against
483 concentration of methane appeared linear over the full range for both temperatures, thus verifying
484 that over the distances sampled within experimental timeframes there is a minimal temperature
485 gradient.

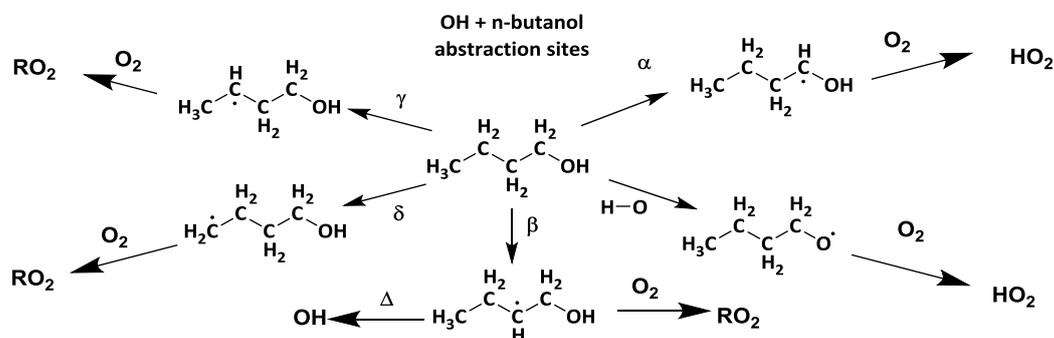


486
487 **Figure 8.** Bimolecular plot for the reaction of OH and methane at 680 K, 1760 Torr using 193 nm
488 photolysis of water as an OH precursor. Here the inset shows that even at removal rates $< 1000 \text{ s}^{-1}$
489 the plot is still linear, indicating that within the measured experimental timescales there is little
490 deviation in temperature.



491 **4 Determination of Site Specific Rate Coefficients for the Reaction of OH with n-butanol**

492 The branching ratios for the sites of OH attack on n-butanol, as presented in Scheme 2, are of
 493 significance to the modelling of the ignition delay times for n-butanol (Agbro et al., 2017).
 494 Abstractions at the α and OH positions are chain terminating reactions at low temperatures due to
 495 the formation of the relatively inert HO_2 radical, and abstraction at the β site leads to chain
 496 propagation, through OH recycling. The new instrument permitted determination of the attack at
 497 the α and β sites; attack at the α site leads to prompt HO_2 formation in the presence of O_2 ; at
 498 elevated temperatures biexponential fits to non-single exponential OH loss traces in the absence
 499 of O_2 (due to decomposition of the β hydroxy radical to OH and iso-butene) allowed for attack at
 500 the β site to be measured.



501

502 **Scheme 2.** The potential sites for OH abstractions in the oxidation of n-butanol. Of particular
 503 importance to low temperature combustion is the ratio of α to β branching fractions where α attack
 504 leads to chain inhibition and beta to chain propagation.

505

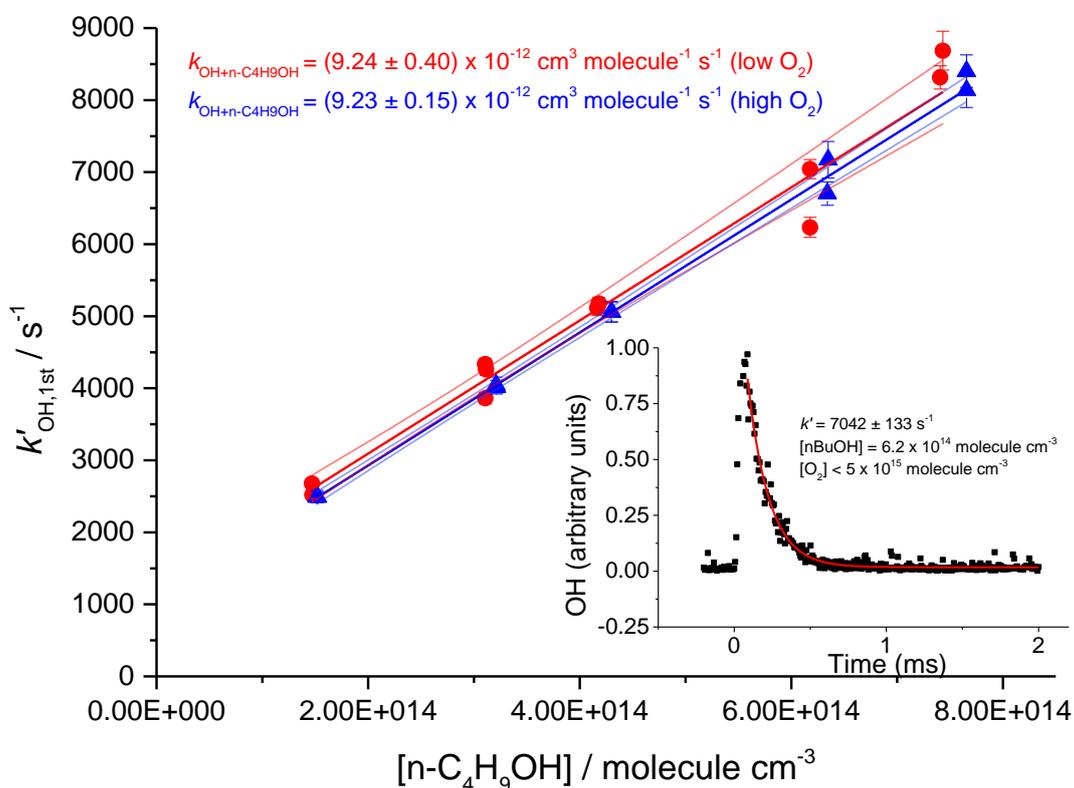
506 **4.1 Room temperature OH kinetics**

507 At room temperature under pseudo-first-order conditions ($[\text{OH}] < 3 \times 10^{12}$ molecule cm^{-3} , [n-
 508 butanol] $> 1.5 \times 10^{14}$ molecule cm^{-3}), the OH loss traces recovered from the first detection axis
 509 from the jet expanded gas corresponded closely with single exponential decays. These decays
 510 relate to the overall loss process for the reaction of OH with n-butanol:





512 The resulting rate coefficients were plotted against the concentration of butanol, in the presence of
 513 both low and high oxygen, as shown in Figure 9 (low oxygen $< 5 \times 10^{15}$ molecule cm^{-3} , high
 514 oxygen 1.2×10^{19} molecule cm^{-3}), where $k_{\text{obs}} = k_1 \times [\text{butanol}]$, giving a resultant bimolecular
 515 removal rate of $k_1 = (9.24 \pm 0.40) \times 10^{-12}$ cm^3 molecule $^{-1}$ s $^{-1}$ under low oxygen conditions, and k_1
 516 $= (9.23 \pm 0.15) \times 10^{-12}$ cm^3 molecule $^{-1}$ s $^{-1}$ under high oxygen conditions.



517 **Figure 9.** Plots $k'_{\text{OH},1\text{st}}$ against the concentration of butanol, at two oxygen concentrations, $< 5 \times$
 518 10^{15} molecule cm^{-3} and 1.2×10^{19} molecule cm^{-3} . Bimolecular rate coefficients were taken from
 519 the slopes as $(9.24 \pm 0.40) \times 10^{-12}$ cm^3 molecule $^{-1}$ s $^{-1}$ under low oxygen conditions (red circles with
 520 95 % confidence limits), and $(9.23 \pm 0.15) \times 10^{-12}$ cm^3 molecule $^{-1}$ s $^{-1}$ under high oxygen conditions
 521 (blue triangles with 95 % confidence limits). The inset shows a typical OH temporal profile at the
 522 first detection axis.
 523

524

525 The good agreement between the measured rate coefficients with varying $[\text{O}_2]$ verifies that,
 526 as expected under our experimental conditions at room temperature, the R radical formed from the
 527 β abstraction does not undergo fragmentation to OH and but-1-ene. The resultant combined data
 528 gives an overall 293 K bimolecular rate coefficient for OH and n-butanol of $k_1 = (9.24 \pm 0.21) \times$



529 $10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$, which is in excellent agreement with the recent work of McGillen et al.
530 (2013) of $k_{1,296} = (9.68 \pm 0.75) \times 10^{-12} \text{ cm}^3 \text{ molecule}^{-1} \text{ s}^{-1}$.

531 4.2 Room temperature HO₂ results

532 Experiments were carried out in high oxygen conditions ($3 \times 10^{17} - 1.2 \times 10^{18} \text{ molecule cm}^{-3}$), at
533 296 – 303 K, and high pressures (1800 – 2000 Torr) of N₂ bath gas using photolysis of hydrogen
534 peroxide at two different wavelengths (248 nm and 266 nm), and the resulting HO₂ yields are
535 shown in Table 2. The resulting HO₂ yield was determined to be $(58 \pm 7) \%$ at 266 nm, and $(55 \pm$
536 $12) \%$ at 248 nm. As there is no significant variation in the yield with laser wavelength or power,
537 we can treat the data in Table 2 as 12 independent estimates of the yield, giving an averaged HO₂
538 yield of 57% with a standard error (95%) of 6%. Therefore under the experimental conditions
539 (pressure >1800 Torr, [O₂] > $3 \times 10^{17} \text{ molecule cm}^{-3}$), the HO₂ yield, which originates from OH
540 attack at the α abstraction site, was $(57 \pm 6) \%$, with a minor contribution from abstraction from
541 the hydroxyl group. The yield assigned is in good agreement with McGillen et al. (2013) 57%, and
542 Cavalli et al. (2002) $52 \pm 7 \%$.

543

544 **Table 2.** HO₂ yields from experiments carried out at room temperature (293 – 298 K) with reaction
545 initiated by photolysis of H₂O₂ at 248 nm and 266 nm.

Laser wavelength/nm	HO ₂ Yield (%)							Average HO ₂ Yield (%)
	Expt 1	Expt 2	Expt 3	Expt 4	Expt 5	Expt 6	Expt 7	
266	61 ± 7	54 ± 4	46 ± 5	56 ± 7	54 ± 7	67 ± 10	66 ± 6	58 ± 7
248	63 ± 2	68 ± 2	48 ± 5	52 ± 5	49 ± 5			55 ± 12

546

547 Experiments were carried out with photolysis at 266 nm and at a variety of laser energies at 248
548 nm, the yields remained consistent with photolysis wavelength and power. Varying the laser power
549 did alter the profiles of the HO₂ traces recovered; the growth rates remained unaffected but the
550 tails changed; decreasing laser power slowed the removal rate of HO₂ (from greater than 100 s^{-1}
551 to under 10 s^{-1}) showing that radical-radical processes are the main source of HO₂ loss from the
552 system. If radical-radical reactions were an important source of any observed HO₂ yield changing
553 laser power would have altered the HO₂ yield and additionally the HO₂ growth kinetics.



554 4.3 Higher temperature – HO₂ yield and OH recycling

555 The R radical formed from abstraction at the β site (CH₃CH₂CHCH₂OH) can regenerate OH and
556 form butene, Scheme 2, in the absence of added oxygen. This process was not observed at ambient
557 temperatures (293 – 305 K) but at elevated temperatures, 616 K – 657 K, the OH loss observed at
558 the first detection axis was no longer well described by a single exponential loss process, Figure
559 10. The non-exponential decays formed were due to OH being returned following decomposition
560 of the β R radical. Biexponential fits to the recycling traces gave the fraction of OH returned
561 (Medeiros et al. 2018), with an average β branching fraction of (23 ± 4)%, Table 3.

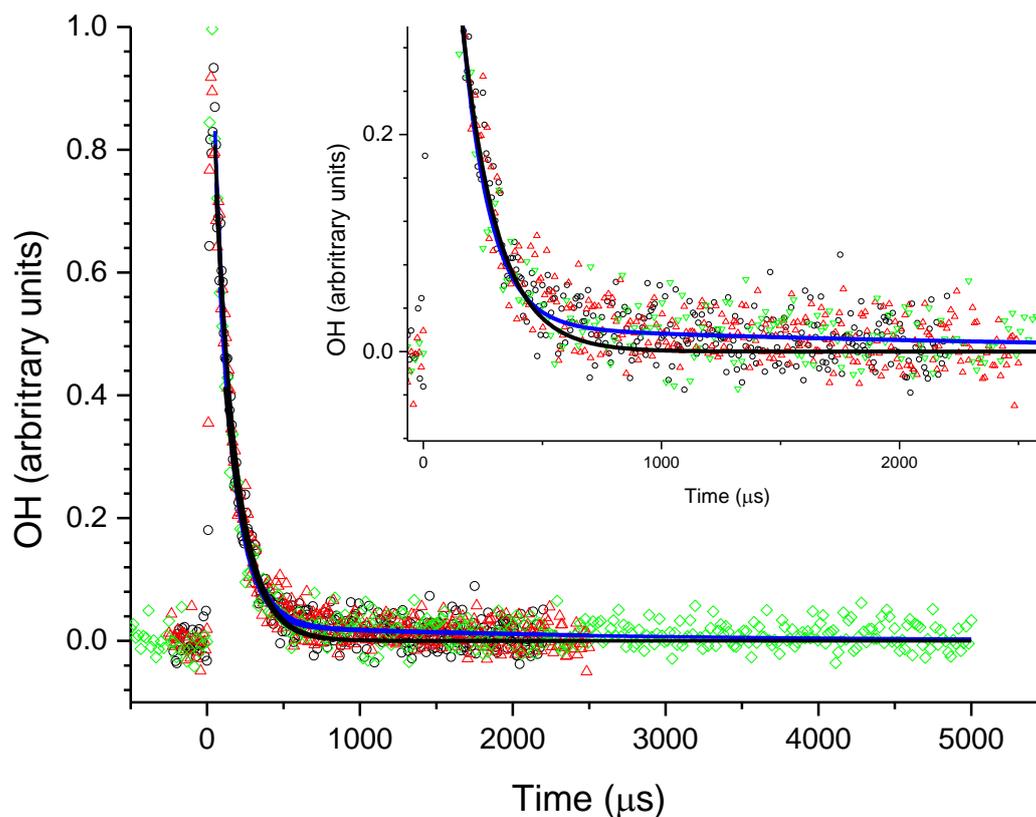
562

563 **Table 3.** OH recycling and HO₂ yields from experiments carried out under elevated temperatures
564 (> 600 K) all experiments were carried out with photolysis at 248 nm.

Temperature (K)	Fraction of OH returned (%)	Observed HO ₂ Yield (%)
616	24.2 ± 4.1	54 ± 4
622	24.4 ± 4.9	
636	25.7 ± 5.6	
657	18.1 ± 4.0	

568

569 The HO₂ yield measured at an elevated temperature (616 K), where OH recycling was also
570 observed, was 54 ± 4 % (Table 3) which is within error of the value (57 ± 6 %) measured at room
571 temperature (293 K), although it is not possible to partition the HO₂ yield between α and OH
572 abstraction. Over the temperature range tested the branching ratio for OH attack at the α position
573 is therefore also likely to remain unchanged. With the sum of the α and β sites contributing (78 ±
574 4)%, at 616 K, the remainder of the abstraction (~22%) occurs at the δ and γ sites. These results
575 are in excellent agreement of the product study of Cavalli et al. (2002) which found (52 ± 7)% α
576 from the butanal product yield and (23 ± 4) % β from the propanal yield using FTIR detection and
577 the site specific analysis by McGillen et al. (57 % α and 26% β). The product study of Hurley et
578 al. (2009) found 44 ± 4 % α and 19 ± 2 % β values which are lower than our experimental values
579 but are within the combined error ranges. However, it should be noted that the β branching fraction
580 of 23 ± 4 % measured in this study was obtained at elevated temperatures, 616 – 657 K.



581

582 **Figure 10.** An example of the OH signal collected at the first detection axis for the reaction of OH
583 with n-butanol ($[n\text{BuOH}] \approx 1.4 \times 10^{15} \text{ molecule cm}^{-3}$, at 616 K. The black line represents the least
584 squares fits to an exponential decay ($k'_{1,1st} = (6780 \pm 380) \text{ s}^{-1}$), with the blue line representing a bi-
585 exponential fit ($k_{1,biexp,1st} = (8190 \pm 180) \text{ s}^{-1}$).

586

587 5 Summary

588 The use of H_2O_2 as an OH precursor has been shown to provide a reliable method of internally
589 characterizing our system for HO_2 yield detection. Interferences that could arise from using this
590 precursor for HO_2 detection have been accounted for, and the presence of water that the H_2O_2
591 precursor introduces has no effect on the sensitivity of the LIF method, unlike IR absorption
592 methods.



593 It has been demonstrated that this instrument can reliably assign HO₂ yields and
594 simultaneously measure OH kinetics, even under conditions of high temperatures and high oxygen
595 concentrations, which could be challenging for other detection systems. Such conditions are
596 important for exploring key combustion chemistry reactions, and for converting slow
597 atmospherically relevant processes to the microsecond timescales required to minimize secondary
598 or heterogeneous chemistry.

599 By performing reactions under low NO_x and low radical densities ($<1 \times 10^{13}$ molecule
600 cm⁻³), HO₂ yields formed on fast timescales (> 300 s⁻¹) can be assigned to direct HO₂ channels or
601 reactions of alkyl (R) radicals with oxygen. Whilst some time-resolution is lost at the HO₂ detector,
602 sufficient time-resolution is retained in order to separate varying sources of HO₂, for example the
603 two channels leading to HO₂ production in the OH/CH₃OH/O₂ system (Section 3.2) or from
604 unwanted secondary chemistry.

605 For particular reactions, illustrated in this paper by the study of OH with methanol and
606 butanol in the presence of oxygen, the simultaneous measurement of OH kinetics and HO₂ yields
607 can provide important site-specific information. In other systems, the onset of HO₂ formation could
608 allow for the assignment of new channels becoming important within complex mechanism,
609 potentially allowing for verifying the onset of OOQOOH chemistry within OH regeneration
610 processes.

611

612 **6 Acknowledgements**

613 A studentship from NERC for T.H. Speak is gratefully acknowledged.

614

615 **7 Author Contributions**

616 THS undertook most of the experimental measurements and contributed to the first draft of the
617 manuscript. DS provided input into experimental design and analysis of transport effects. MAB
618 and PWS lead the project and completed the manuscript.

619



620 8 Competing Interests

621 The authors declare that they have no conflicts of interest.

622

623 9 References

624

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